

ARTICLE

https://doi.org/10.1038/s41467-020-16674-y

OPEN

Harnessing strong metal-support interactions via a reverse route

Peiwen Wu^{1,2,10}, Shuai Tan^{1,10}, Jisue Moon¹, Zihao Yan³, Victor Fung⁴, Na Li^{5,6}, Shi-Ze Yang¹, Yongqiang Cheng⁷, Carter W. Abney¹, Zili Wu¹, Aditya Savara¹, Ayyoub M. Momen⁸, De-en Jiang⁴, Dong Su⁵, Huaming Li², Wenshuai Zhu², Sheng Dai^{1,9} & Huiyuan Zhu¹,^{1,3}

Engineering strong metal-support interactions (SMSI) is an effective strategy for tuning structures and performances of supported metal catalysts but induces poor exposure of active sites. Here, we demonstrate a strong metal-support interaction via a reverse route (SMSIR) by starting from the final morphology of SMSI (fully-encapsulated core-shell structure) to obtain the intermediate state with desirable exposure of metal sites. Using core-shell nanoparticles (NPs) as a building block, the Pd-FeO_x NPs are transformed into a porous yolk-shell structure along with the formation of SMSIR upon treatment under a reductive atmosphere. The final structure, denoted as $Pd-Fe_3O_4-H$, exhibits excellent catalytic performance in semi-hydrogenation of acetylene with 100% conversion and 85.1% selectivity to ethylene at 80 °C. Detailed electron microscopic and spectroscopic experiments coupled with computational modeling demonstrate that the compelling performance stems from the SMSIR, favoring the formation of surface hydrogen on Pd instead of hydride.



¹ Chemical Sciences Division, Oak Ridge National Laboratory, Oak Ridge, TN 37831, USA. ² School of Chemistry & Chemical Engineering, Jiangsu University, Zhenjiang 212013, China. ³ Department of Chemical Engineering, Virginia Polytechnic Institute and State University, Blacksburg, VA 24061, USA. ⁴ Department of Chemistry, University of California, Riverside, CA 92521, USA. ⁵ Center for Functional Nanomaterials, Brookhaven National Laboratory, Upton, NY 11973, USA. ⁶ Frontier Institute of Science and Technology, Xi'an Jiaotong University, Xi'an 710054, China. ⁷ Neutron Scattering Division, Oak Ridge National Laboratory, Oak Ridge, TN 37831, USA. ⁸ Energy and Transportation Science Division, Oak Ridge National Laboratory, Oak Ridge, TN 37831, USA. ⁹ Joint Institute for Advanced Materials, University of Tennessee, Knoxville, TN 37996, USA. ¹⁰These authors contributed equally: Peiwen Wu, Shuai Tan. ^{Se}email: zhuws@ujs.edu.cn; dais@ornl.gov; huiyuanz@vt.edu

upported metal catalysts have long been recognized as the most important group of heterogeneous catalysts for fundamental investigations and modern chemical industries¹⁻⁴. Conventionally, these catalysts are synthesized by anchoring the active metal nanoparticles (NPs) onto certain high-surface-area supports to increase the dispersion of catalytically active sites and stabilize the metal against leaching⁵⁻⁷. Subsequently, the metal-support interface is constructed. Such an interface provides synergistic properties to regulate catalysis by modifying the electronic (charge transfer between the metal sites and the support) and/or geometric (decoration or coverage of metal sites by the support) parameters, and also by modulating the reaction pathways, e.g., lattice oxygen in oxide supports may directly participate in catalytic reactions⁷; multicomponent interfaces can enable tandem reaction pathways that do not exist on singlecomponent active sites^{8,9}.

As a classic prototype in metal-support interactions, the strong metal-support interaction (SMSI) has been defined as the encapsulation of NPs, usually group VIII metals, by partially reduced oxide supports during high-temperature hydrogen (H₂) treatment^{10,11}. Since the very first discovery of SMSI by Tauster et al.¹²⁻¹⁴, SMSI has been widely exploited to tune catalytic performances of group VIII NPs by engineering geometric and/or electronic structures of these metal sites. For example, the adsorption of H₂ or CO on Pd was extremely suppressed upon the formation of SMSI (refs. 13,15), suggesting that the active metal sites were largely covered by support, which altered the geometric ensembles and improved the thermal stability of Pd catalysts. Meanwhile, because the reducible oxide support, e.g., TiO₂, Co₃O₄, CeO₂, and Nb₂O₅, is partially reduced to the structure with a nonstoichiometric oxygen concentration during the reductive annealing, electron transfer between metal NPs and oxide supports was detected¹⁶⁻¹⁹. Under extreme conditions, the formation of intermetallic structure of the supported metal and metal cations in the supporting oxide was observed^{20,21}.

Despite these fascinating interfacial properties in SMSI, the formation of SMSI is restricted to specific combinations of elements, i.e., group VIII metals with high surface energy and transition metal oxides with low surface energy. Consequently, it is extremely challenging for some metals, e.g., Au, to manifest SMSI due to their low work function and surface energy^{15,17,22}.

Efforts have been devoted in hope of expanding upon the conventional SMSI. One critical element in this pursuit is switching the high-temperature treatment in H₂ into other conditions and thereby changes the mechanistic pathways for the formation of SMSI. For example, Wang et al. reported SMSI formation between Au NPs and TiO₂ induced by melamine under an oxidative atmosphere. With the formation of SMSI, the Au NPs were encapsulated by a permeable TiO_x thin layer, making the Au NPs ultrastable at 800 °C (ref. ²³). Xiao et al. reported a wet chemistry approach to construct SMSI in aqueous solution at room temperature, which was realized by engineering redox interactions between metals and supports. This strategy was applicable to Au, Pt, Pd, and Rh (ref. 15). Christopher et al. developed a strongly bounded-adsorbate-mediated strategy to construct SMSI between Rh and TiO₂ through high-temperature treatment in the mixture of CO_2 and H_2 (ref. ²⁴). Zhang et al. engineered the SMSI between Au NPs and hydroxyapatite by treating the Au NP-hydroxyapatite composite in the air at high temperatures¹⁷. Although progress has been made in expanding the boundaries of SMSI, one inevitable issue associated with the conventional SMSI is that upon high-temperature treatment the encapsulation process immediately and uncontrollably takes place, resulting in limited exposure of active sites²⁵. In the ideal scenario, the oxide coverage on the metal surface needs to be thin and permeable to small molecules, while still fully encapsulating metal NPs to prevent the dissolution, disintegration, and aggregation of active sites during catalysis.

We recently reported that voids and cavity space can be developed in metal-metal oxide core-shell NPs in response to H_2 treatment at 200 °C (ref. ²⁶). This observation combined with the current issues in conventional SMSI motivated us to develop alternative routes to metal-support interactions. Here, we denote this type of structural rearrangement as the strong metal-support interaction via a reverse route (SMSIR). Specifically, we start from the final morphology of SMSI (full encapsulation) and end in the intermediate state with partial exposure of metal sites (Fig. 1). As a proof of concept, we demonstrate that the core-shell Pd-FeO_x NPs can be restructured into a porous yolk-shell structure after optimized reductive annealing (Pd-Fe₃O₄-H). Characterizations reveal that Pd atoms gradually migrate into the Fe₃O₄. The



Fig. 1 Schematic illustration of the formation of strong interactions. a The conventional SMSI formation process. b The SMSIR formation process in this work.

Pd–Fe₃O₄–H shows 100% conversion and 85.1% selectivity in the acetylene (C_2H_2) semi-hydrogenation at atmospheric pressure and a mild reaction temperature of 80 °C. Further investigations demonstrate that the Pd–Fe₃O₄–H engineered by the SMSIR alleviates the strong H₂ adsorption on Pd sites, in favor of the formation of surface hydrogen (surface-H) instead of hydride during the hydrogenation of C_2H_2 to C_2H_4 . Our results on the scenario of engineering SMSIR can help to circumvent the current limits in metal–support interfaces, expanding the boundaries of conventional SMSI, and providing opportunities to rationally maneuver structure-dependent catalytic outcomes.

Results

Synthesis and characterization. Details of the material synthesis can be found in the "Methods" section. Briefly, the Pd NPs with a size of 5.5 ± 0.5 nm (Supplementary Fig. 1) were prepared by the reduction of palladium (II) acetylacetonate (Pd(acac)₂) in oleylamine (OAM) as modified from a previous report²⁷. The core-shell Pd-FeO_x NPs were obtained by a seed-mediated growth method with the pre-made Pd NPs as the seeds and iron (III) acetylacetonate, as the iron precursor that nucleated on Pd surface, forming an iron oxide shell. The pristine core-shell sample was denoted as Pd-FeO_x NPs (Supplementary Figs. 2 and 3). The SMSIR was constructed by treating the Pd-FeO_x NPs at 300 °C in a gas mixture of H₂ and argon (Ar; 4 vol.% of H₂), and the sample was named as Pd-Fe₃O₄-H. As a comparison, the Pd-FeO_x NPs were treated in the air at 300 °C to obtain the structure without SMSIR (Pd-Fe₃O₄-A).

X-ray diffraction (XRD) was performed to determine the crystal structures of the samples. As shown in the XRD patterns of pristine Pd–FeO_x and Pd–Fe₃O₄–A (Supplementary Fig. 4), characteristic peaks at $2\theta = 40.1^{\circ}$ with very low intensities were detected, which can be assigned to the (111) peak of face-centered cubic (*fcc*) Pd. No additional peaks in the XRD patterns can be found, indicating the amorphous nature of iron oxide shell in both pristine Pd–FeO_x and Pd–Fe₃O₄–A. On the contrary, in the

XRD pattern of Pd–Fe₃O₄–H, the intensity of Pd (111) peak increases remarkably, and a series of characteristic peaks at 2θ = 30.6°, 35.9°, 43.5°, 53.9°, 57.3°, 63.0°, and 74.3° are clearly observed, which can be assigned to (220), (311), (400), (422), (511), (440), and (533) lattices of γ -Fe₃O₄. The XRD characterization indicates that annealing in the reductive atmosphere may facilitate the spatial redistribution of grains in the oxide shell, and promotes the crystallization of Pd and iron oxides, consistent with our previous report²⁶.

The aberration-corrected high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) images of the Pd-Fe₃O₄-H in Fig. 2a show that the core-shell structure of pristine Pd-FeOx NPs evolved into a unique porous yolk-shell structure after reductive annealing at 300 °C. Magnified HR-STEM images of Pd-Fe₃O₄-H in Fig. 2b, c demonstrate a lattice parameter of 0.217 nm in the core, corresponding to the (111) plane of Pd, and lattice parameters of 0.251 and 0.146 nm in the shell, corresponding to the (311) and (440) planes of Fe₃O₄. More interestingly, the magnified HR-STEM image in Fig. 2d shows that there are abundant voids, i.e., lattice vacancies, in the Fe₃O₄ shells (marked in yellow circles). To analyze the pore distribution, the pore sizes were determined by averaging pore sizes in multiple HR-STEM images (Supplementary Fig. 5). The majority of these pores on the Fe₃O₄ shell are micropores with an average pore size of 0.73 nm. Furthermore, electron energy loss spectroscopy (EELS) mapping of Pd-Fe₃O₄-H in Fig. 2e-i depict a yolk-shell-like structure of Pd yolk and Fe₃O₄ shell with numerous voids. In contrast, for Pd-Fe₃O₄-A, no significant voids were detected in the Fe₃O₄ shells and the intact core-shell structure was retained (Supplementary Fig. 6). It is known that the reducible metal oxides can be partially reduced after high-temperature treatment in H₂ (ref. 28). H₂ reacts with these oxides to produce water and generate oxygen vacancies in the oxide matrix. This process can be further facilitated by platinum-group metal NPs supported on those oxides through a H₂ spillover process^{29,30}. In the meantime, the crystallization of oxide shell could promote the rearrangement of



Fig. 2 STEM characterization of the Pd-Fe₃O₄-H sample. a HAADF-STEM image of Pd-Fe₃O₄-H and schematic illustration of the structure (the yellow shell stands for Fe₃O₄, and grey core stands for Pd); **b** HR-STEM images of Pd core, **c** Fe₃O₄ shell, and **d** Pd-Fe₃O₄-H (voids in oxide shell are marked in yellow circles); **e** STEM image of Pd-Fe₃O₄-H at lower magnification; **f**-**i** corresponding EELS elemental mappings of the selected section in **e**; **f** Fe, **g** Pd, **h** O, and **i** overlapped figure.



Fig. 3 XAFS characterization of prepared samples and reference samples. a Pd K-edge EXAFS; b Pd K-edge XANES; c Fe K-edge EXAFS; and d Fe K-edge XANES. Source data are provided as a Source data file.

atoms, alter the distribution of oxide grains to expand the generated oxygen vacancies, and finally develop voids and cavity space in the structure.

slightly oxidized by air, consistent with our EXAFS and XANES results in Fig. 3.

XAFS characterization and simulations. To understand the coordination environments of Pd-Fe₃O₄ structures, X-ray absorption near-edge spectroscopy (XANES) and extended Xray absorption fine structure (EXAFS) were performed (Fig. 3, Supplementary Tables 1 and 2). The chemical states of Pd in Pd-Fe₃O₄-H and Pd-Fe₃O₄-A samples were investigated in Pd K-edge EXAFS and XANES, and Pd foil was employed as a reference (Fig. 3a, b, Supplementary Table 1). The Pd in Pd-Fe₃O₄-H mainly exists in the form of metallic Pd⁰, while in Pd–Fe₃O₄–A, Pd demonstrates an oxidized feature to some extent. To determine the chemical states and structures of iron oxide shells, the Fe K-edge EXAFS (Fig. 3c), corresponding fitting (Supplementary Table 2), the Fe K-edge XANES (Fig. 3d), and the Fe K-edge first derivative XANES (Supplementary Fig. 7) were collected and analyzed. Compared with the Fe₃O₄ and Fe₂O₃ references, the Fe K-edge XANES and the Fe K-edge first derivative XANES indicated that the oxide shell in Pd-Fe₃O₄-H was similar to Fe₃O₄, while the oxide shell in Pd-Fe₃O₄-A possessed a partially oxidized Fe₃O₄ feature (Fig. 3d, Supplementary Fig. 7).

Because Pd–Pd and Pd–Fe bond lengths are similar, it is hard to visualize the difference between these two bonds with Fourier transform results. In this regard, the wavelet transform (WT) EXAFS as a powerful technique was employed to distinguish these two bonds in our samples. It can be clearly seen from Fig. 4a, b that compared with the standard WT EXAFS images for Pd–Fe, Pd–O, Pd–Pd, and Pd foil (Supplementary Fig. 8), the Pd in Pd–Fe₃O–H remains to be the metallic Pd⁰ state and Fe–Pd bond emerges (Fig. 4a). In contrast, for the Pd–Fe₃O₄–A sample (Fig. 4b), the result demonstrates an oxidized feature with the formation of the Pd–O bond, indicating that the Pd may be

Density functional theory (DFT) simulations combined with the EXAFS curve fitting were carried out to provide more insight into the crystal structure of iron oxide, and the interactions between Pd and Fe₃O₄. First, a series of models including a Pd cluster atop the surfaces of Fe₂O₃ and Fe₃O₄, and a Pd cluster in oxygen vacancy of Fe₂O₃, and Fe₃O₄ surfaces were constructed and optimized by DFT in Supplementary Fig. 9, and the corresponding FEFF calculated scattering paths were also presented (Supplementary Tables 3-5). Then, the EXAFS curve fitting on the DFT-optimized structures (Supplementary Figs. 10 and 11, Supplementary Tables 6 and 7) of both Pd K-edge EXAFS and Fe K-edge EXAFS were obtained. It can be concluded from the results that the best-fitted structure of Pd-Fe₃O₄-H is that the Pd atoms intercalate into the Fe₃O₄ matrix (Fig. 4c, detailed optimizing process see Supplementary Fig. 10), indicating that the Pd enters into the Fe₃O₄ lattice, substituting an oxygen vacancy and tends to form the Fe-Pd bond with Fe in Fe₃O₄. This observation suggests that there exist strong interactions between Pd and Fe₃O₄ in Pd-Fe₃O₄-H. In contrast, the Pd-Fe₃O₄-A demonstrated a good match to the local geometry of Pd atoms situated on the surface of Fe₃O₄ (Fig. 4d, detailed optimizing process see Supplementary Fig. 11). This result may shed some light on the formation mechanism of this unique porous yolk-shell structure. Evidently, the reaction between H₂ molecules and O atoms in the Fe_3O_4 could generate oxygen vacancies in the structure upon evaporating the produced water. Meanwhile, the crystallization of the oxide shell and the new Fe-Pd bond formation could promote the rearrangement of oxide lattice and the mobility of Pd atoms, expanding the atom vacancies and developing cavity space in the structure.

XPS and DRIFTS investigations. To investigate the charge transfer with the formation of SMSIR, X-ray photoelectron



Fig. 4 Pd K-edge WT EXAFS and EXAFS fitting using DFT-optimized results. a Pd K-edge WT EXAFS of Pd-Fe₃O₄-H; **b** WT EXAFS of Pd-Fe₃O₄-A; **c** EXAFS curve fitting on DFT-optimized Pd-Fe₃O₄-H model; and **d** EXAFS curve fitting on DFT-optimized Pd-Fe₃O₄-A model. Source data are provided as a Source data file.

spectroscopy (XPS) and CO diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) were carried out and shown in Supplementary Figs. 12-14. In the high-resolution Pd 3d XPS of Pd-FeO_x NPs, only a Pd $3d_{5/2}$ peak at 335.4 eV, being assigned to metallic Pd, was found^{31,32}. When the Pd–FeO_x NPs were treated in air at 300 °C, an additional Pd $3d_{5/2}$ peak at 336.8 eV assigned to PdO, emerged in Supplementary Fig. 12. This observation is consistent with our XAFS results that the Pd in Pd-Fe₃O₄-A possesses an oxidized feature to some extent. Furthermore, a Pd $3d_{5/2}$ shoulder peak at 336.2 eV in the high-resolution Pd 3d XPS of Pd-Fe₃O₄-H was detected and assigned to the positively charged Pd $(Pd^{\delta+})^{33}$, which is originated from intercalation of Pd into Fe₃O₄ matrix, leading to the strong interactions between Pd and Fe to form Pd-Fe bond³⁴, in accordance with the XAFS results. Meanwhile, in the high-resolution Fe 2p XPS of Pd-Fe₃O₄-H (Supplementary Fig. 13), the peaks of Fe $2p_{1/2}$ and Fe $2p_{3/2}$ downshifted comparing with that of Pd-Fe₃O₄-A, further confirming that the charge transfers from Pd to Fe₃O₄ in Pd-Fe₃O₄-H. The XPS results indicate the formation of strong interactions and partial electron transfer between Pd and Fe₃O₄. The CO DRIFTS was further carried out. During the test, we found that the CO adsorption peak was weak. We, therefore, subtracted the pure gas-phase signal from each data set. As shown in Supplementary Fig. 14, a peak at ~2153 cm⁻¹ was detected both in the CO DRIFTS of Pd-Fe₃O₄-H and Pd-Fe₃O₄-A, which is assigned to Fe³⁺-CO (ref. ³⁵). Due to the core-shell morphology of Pd-Fe₃O₄-A where Pd is fully encapsulated by Fe₃O₄, no obvious peak was detected in the CO DRIFTS of Pd-Fe₃O₄-A. In contrast, a very weak peak at 2102 cm^{-1} can be seen in the CO DRIFTS of Pd-Fe₃O₄-H, which is assigned to the linear CO adsorption on metallic Pd (ref. ³⁶). More interestingly, an additional peak at 2134 cm^{-1} can be found. Compared with the linear

CO adsorption on metallic Pd, this blueshifted peak is assigned to linear CO adsorption on positively charged Pd (CO–Pd $^{\delta+}$)³⁷. Combined with the XPS analysis, this peak may be attributed to the linear CO adsorption on Pd $^{\delta+}$ in the newly emerged Pd–Fe bond of Pd–Fe₃O₄–H.

The Pd-Fe₃O₄-H sample was further re-treated in air at 300 °C to obtain the Pd-Fe₃O₄-Re sample, and characterized by TEM, CO DRIFTS, and XPS to determine the reversibility of SMSIR. As shown in the TEM image of the Pd-Fe₃O₄-Re (Supplementary Fig. 15), the sample still possesses a yolk-shell structure, but the voids are smaller than those of Pd-Fe₃O₄-H. The XPS of Pd-Fe₃O₄-Re (Supplementary Fig. 16) demonstrates three Pd states of metallic Pd, $Pd^{\delta+}$ in Pd–Fe bond, and PdO. The intensity of $Pd^{\delta+}$ peak is lower than that of $Pd\-Fe_3O_4\-H$ (Supplementary Fig. 12), indicating the decrease of $Pd^{\delta+}$ concentration. The CO DRIFTS of Pd-Fe₃O₄-Re in Supplementary Fig. 17 shows that the intensity of CO-Pd^{δ +} became weaker than that in the CO DRIFTS of Pd-Fe₃O₄-H in Supplementary Fig. 14, suggesting the CO DRIFTS spectral feature is an intermediate state between Pd-Fe₃O₄-H and Pd-Fe₃O₄-A. The analysis of TEM, CO DRIFTS, and XPS together suggests that the SMSIR in this work is partially reversible.

Catalytic performance. The semi-hydrogenation of C_2H_2 to C_2H_4 is an important reaction in industrial purification of the C_2H_4 stream produced from naphtha cracking. Pd-based catalysts are mostly used for this reaction with a consensus that the selectivity is sensitive to the structure of the catalyst³⁸. H₂ molecules that are weakly adsorbed onto the Pd surface to form surface-H and C_2H_2 molecules that are strongly adsorbed can lead to the production of C_2H_4 , while the formation of hydride



Fig. 5 Catalytic performances of the prepared samples for the semi-hydrogenation of C_2H_2 **. a** The comparison of catalytic performance of different systems; **b** light-off curves of the Pd-Fe₃O₄-H catalyst; **c** stability of Pd-Fe₃O₄-H under high conversion. Reaction conditions: *m* (catal.) = 15 mg; *v* (gas) = 50 sccm (0.6 sccm C₂H₂, 3 sccm H₂, 46.4 sccm He). The reaction temperature in **a** and **c** is 80 °C. Error bars represent the instrumental error (±10 %). Source data are provided as a Source data file.

usually results in the total hydrogenation to ethane (C_2H_6). The adsorption of H_2 and C_2H_2 strongly relies on the structure of Pd catalysts. Herein, the hydrogenation of C_2H_2 was systematically investigated over the prepared catalysts to correlate their structural properties with the catalytic outcomes.

As shown in Fig. 5a, Pd NPs totally converted C₂H₂ to C₂H₆ without any selectivity toward C2H4 at 80 °C, while Fe3O4 NPs treated at 300 °C in a gas mixture of H₂ and Ar (4 vol.% of H₂; Fe₃O₄-H) barely demonstrated any catalytic activity for the hydrogenation of C₂H₂. The selectivity of C₂H₂ to C₂H₄ over the Pd-Fe₃O₄-A was 100%, but the conversion was only 25.6%. This observation can be mainly attributed to the core-shell structure of the Pd-Fe₃O₄-A that only exposes limited active Pd sites through the amorphous oxide shell, restricting the adsorption of the reactants. When the Pd-Fe₃O₄-H was employed in the semi-hydrogenation of C₂H₂ at 80 °C, the conversion was 100% and the selectivity was as high as 85.1%. The light-off curves of Pd-Fe₃O₄-H (Fig. 5b) demonstrate that the conversion of C_2H_2 increases with the increment of reaction temperature, while the selectivity toward C₂H₄ shows the opposite trend. To comprehensively compare the catalytic performance between the Pd-Fe₃O₄-H catalyst and previously reported values, the turnover frequency (TOF) was calculated based on the dispersion of Pd (obtained from H₂-pulse chemisorption in Supplementary Table 8). The TOF of Pd-Fe₃O₄-H was 6.46 s^{-1} , ~100-fold higher than those of a series of state-of-the-art single-atom catalysts at 80 °C (Supplementary Fig. 18), indicating that the Pd-Fe₃O₄-H demonstrated compelling catalytic performance for semi-hydrogenation of C₂H₂. Stability tests of the Pd-Fe₃O₄-H catalyst were further carried out under both the high and low conversion rates (Fig. 5c, Supplementary Fig. 19). Both results show that the Pd-Fe₃O₄-H catalyst was remarkably stable in the semi-hydrogenation of C₂H₂ to C₂H₄, which could be originated from the SMSIR between Pd and Fe₃O₄.

The formation of hydride in Pd-based catalysts is temperaturesensitive, and it dominates the total hydrogenation of C_2H_2 (refs. ^{38,39}). Hence, the dispersion of Pd is determined by H₂pulse chemisorption (Supplementary Table 8) at various temperatures to examine the formation of hydride. For the reference Pd NPs (commercial 5 wt.% Pd/Al₂O₃), the dispersion was determined to be 7.6% at -130 °C (cold bath of isopentane and liquid N₂). The corresponding particle size was calculated to be 14.8 nm. However, H₂ uptake on Pd NPs increased significantly at 35 °C, and the estimated particle size decreased to 1.6 nm. This discrepancy can be attributed to the substantial formation of hydride on Pd NPs at higher temperature that interferes with the estimation of particle size⁴⁰. In contrast, the Pd-Fe₃O₄-H sample demonstrated a dispersion of 26.7 and 24.4% at -130 and 35 °C, respectively. The corresponding particle sizes were calculated to be 4.2 and 4.6 nm, in agreement with the Pd core size from STEM investigations (Fig. 2). These observations indicate that the formation of hydride may be effectively inhibited in our Pd-Fe₃O₄-H catalyst with SMSIR, leading to a superior selectivity toward semi-hydrogenated products in the catalytic investigations.

Control experiments. A series of control samples obtained at different treating temperatures (T200, T300, and T400) were prepared (see "Methods" section) to determine the optimized condition for the formation of SMSIR. Here, the T300 stands for the Pd-Fe₃O₄-H sample with SMSIR. The structures and compositions of all catalysts are characterized by TEM, STEM (Supplementary Figs. 20 and 21), EXAFS, XANES, EXAFS curve fitting on DFT-optimized model (Supplementary Figs. 22-29, Supplementary Tables 9-11), and XRD patterns (Supplementary Fig. 30). The corresponding structures are summarized here: in the pristine core-shell Pd-FeO_x sample, the core and shell were metallic Pd⁰ and amorphous Fe_3O_4 . When the sample was treated in the air at high temperature (Pd-Fe₃O₄-A), the core-shell structures maintained with no obvious formation of voids. When the Pd-FeOx NPs sample was treated in H₂ at different temperatures, the core and shell crystallized into Pd⁰ and Fe₃O₄, respectively. As a result,

the T200 demonstrated a core-shell structure with fewer voids, T300 (Pd-Fe₃O₄-H) embraced a yolk-shell-like structure with numerous voids, and the T400 showed a heterostructure of Fe₃O₄ islands on Pd NPs. Especially, it can be seen from the EXAFS and corresponding fitting results of T300, i.e., Pd-Fe₃O₄-H, (Fig. 3c, Supplementary Table 2) that compared with the sample obtained at lower annealing temperatures (T200 sample; Supplementary Fig. 24, Supplementary Table 10), the Fe-O coordination number decreased but Fe-Fe coordination number remained stable in Pd-Fe₃O₄-H. This result further suggests that in Pd-Fe₃O₄-H, Pd may substitute the oxygen in iron oxide and form a new Fe-Pd bond, indicating the formation of strong interactions between Pd NPs and Fe₃O₄ shell. In addition, Pd-FeO_x NPs with different shell thicknesses (STs) were also prepared. With the increment of STs, the samples were denoted as ST1 NPs, ST2 NPs (i.e., Pd-FeO_x NPs), and ST3 NPs, and the NPs were further loaded onto y-Al₂O₃ to obtain ST1, ST2 (i.e. Pd-Fe₃O₄-H), and ST3 (for characterizations see Supplementary Figs. 31-34). To help understand the structures of all prepared samples, a schematic diagram was presented in Supplementary Figs. 35 and 36.

To highlight the role of SMSIR in tuning the conversion and selectivity of C₂H₂ semi-hydrogenation, both sets of control samples were employed in the C_2H_2 semi-hydrogenation reaction. As shown in Supplementary Figs. 37 and 38, the Pd-Fe₃O₄-H, i.e., T300 and ST2, demonstrates the best catalytic performance. This result further reveals that the optimized ST and treating condition are essential to the formation of SMSIR for the promoted semihydrogenation of C₂H₂ to C₂H₄. Based on the structures of the catalysts, the different catalytic outcomes can be attributed to the following factors: (1) regarding the effect of annealing temperatures, all samples possess a similar Pd size, indicating that the difference of catalytic performance is not originated from the difference of particle sizes (Supplementary Fig. 39). In the T200sample, there are fewer voids in the oxide shell and the T200 remains to be a core-shell structure, resulting in poor exposure of Pd active sites with limited activity. In the case of T400 sample, the core-shell structure is completely destroyed, and therefore the formation of hydrides turns to be favorable because of the loss of core-shell structural confinement; (2) for the effect of ST, a thicker shell in ST3 makes the Pd active sites less exposed. However, when the shell becomes too thin as the case in ST1, the structure cannot maintain a fully-encapsulated state, but rather more like a heterostructure with some iron oxide islands on Pd NPs. Consequently, Pd domains tend to form hydrides due to the lack of core-shell structural confinement effect.

Reaction mechanism. The reaction kinetics were further explored to understand the underlying mechanisms. As shown in Supplementary Fig. 40, the reaction order over C_2H_2 is calculated to be -1 (up to 2.5% atm partial pressure), roughly in agreement with Monnier's work with ~ -0.7 reaction order⁴¹, indicating the strong adsorption of C₂H₂ on the surface of Pd in the Pd-Fe₃O₄-H catalyst. There exists a debate regarding the H₂ reaction order. In general, the reaction order varies from ~0.5 (refs. 42,43), ~1 (refs. 44,45), and up to ~1.6 (ref. 46). In our work, we found the reaction order of H_2 to be ~2 (up to 10% atm partial pressure). Such a positive dependence on H₂ partial pressure indicates a much weaker H₂ adsorption than previous studies. The temperature dependence of the Pd-Fe₃O₄-H sample was investigated at 1.2%/6% atm partial pressure of C2H2/H2 (Supplementary Fig. 41). The apparent activation energy was found to be \sim 52.7 kJ mol^{-1} , in good agreement with Monnier's 12.1 kcal mol^{-1} (ref. ⁴¹) and Zhang's $52 \text{ kJ} \text{ mol}^{-1}$ (ref. ⁴⁵).

The inelastic neutron scattering (INS) spectra of H_2 adsorption on Pd–Fe₃O₄–H and bulk Pd were presented in Fig. 6. The signal of H₂-sorption behavior in Pd–Fe₃O₄–H is totally different from that in bulk PdH_x. In bulk PdH_x sample, an evident signal of hydride was detected, while in Pd–Fe₃O₄–H, the signal of hydride was very weak^{47,48}. The profile of the peak at 500 cm⁻¹ reflects the status of the hydride. Specifically, the sharp peak followed by a shoulder as seen in bulk PdH_x is due to certain dispersion relation of optical phonons in 3D space, which results in this particular distribution of phonon states. When hydride is only formed at or near the surface, the 3D network is lacking, leading to the broad bump in the spectrum of our Pd–Fe₃O₄–H sample. The result indicates that only surface-H formed during the reaction process, consistent with our H₂-chemisorption results.

Discussion

In this work, we reported a strategy to engineer the SMSI between Pd and Fe₃O₄ by using core-shell NPs as a building block through a reverse process of the formation of conventional SMSI, denoted as SMSIR. With the formation of SMSIR, the core-shell Pd-FeO_x NPs was restructured into a unique porous yolk-shell structured Pd-Fe₃O₄-H, in favor of the exposure of Pd active sites. The Pd-Fe₃O₄-H with SMSIR demonstrated excellent catalytic performance in semi-hydrogenation of C₂H₂ to C₂H₄ with 100% conversion, 85.1% selectivity, and a high TOF of 6.46 s⁻¹ at the reaction temperature as low as 80 °C. XAFS investigations along with DFT simulations verified that the Pd atoms intercalate into the Fe₃O₄ matrix and form strong interactions. The electron transfer was probed by CO DRIFTS and XPS, suggesting that with the formation of SMSIR, electrons partially transfers from Pd to Fe₃O₄ shell. The optimized ST of Pd-FeO_x NPs and annealing temperature were found to be essential to the formation of SMSIR. Detailed mechanistic investigations indicated that the SMSIR in Pd-Fe₃O₄-H alleviates the strong chemisorption of H₂ on Pd sites, prevents the formation of hydride, and consequently leads to a superior selectivity toward C₂H₄. This work not only develops a high-performance catalyst for semi-hydrogenation of C₂H₂ but also provides an approach for the construction of effective catalytic structures based on unconventional SMSI.

Methods

Chemicals. $Pd(acac)_2$ (>99.99%), OAM (90%), tri-n-octylphosphine (TOP, AR.), hexane (AR.), ethanol (AR.), ferric (III) acetylacetonate (Fe(acac)_3, >99.99%), and *y*-Al₂O₃ were obtained from Sigma Aldrich Corporate (USA) without further purification.

Preparation of 4 nm Pd NPs. The Pd NPs were prepared by a modified method from previous work as following²⁷: 70 mg of Pd(acac)₂ was mixed with 15 mL of OAM in a 100 mL of four-neck flask under stirring. The mixture was then heated to 80 °C at a ramping rate of 5 °C min⁻¹ and kept for 1 h under the protection of N₂. A total of 0.5 mL of TOP was added to the solution. The mixture was further heated to 250 °C at a ramping rate of 5.6 °C min⁻¹, and kept at this temperature for another 1 h before cooling down to room temperature. Subsequently, the mixture was transferred to a 50 mL of centrifuge tube, and 30 mL of ethanol was added. The Pd NPs were separated by centrifugation at $4656 \times g$ for 10 min. Then, the Pd NPs were redispersed in 10 mL of hexane, and precipitated and washed by adding 30 mL of ethanol for two times. Finally, the Pd NPs were dispersed in 10 mL of hexane for further use.

Preparation of Pd-FeO_x NPs. A total of 110 mg of Fe(acac)₃ and 20 mL of OAM were added to a 100 mL four-neck flask. The mixture was heated to 90 °C at a ramping rate of 5 °C min⁻¹ in N₂. Subsequently, 12.5 mg of Pd NPs were added, followed by heating to 250 °C and kept there for 30 min. Afterward, the reaction temperature was raised to 300 °C and kept there for another 30 min before naturally cooling to room temperature. Then, 30 mL of ethanol was added to precipitate the Pd-FeO_x NPs, and then centrifuged at 4656 × *g* for 10 min. The Pd-FeO_x NPs was redispersed in 10 mL of hexane and washed by 30 mL of ethanol for two times. Finally, the Pd-FeO_x NPs were dispersed in 10 mL of hexane.

Preparation of FeO_x NPs. The synthesis of FeO_x NPs is the same as the preparation of Pd–FeO_x NPs, without adding Pd NPs.



Fig. 6 Determination of reaction intermediate species over Pd-Fe₃O₄-H and bulk PdH_x. a INS spectra of Pd-Fe₃O₄-H and bulk PdH_x. **b** schematic diagram of surface-H formed in Pd-Fe₃O₄-H; and **c** schematic diagram of hydride formed in bulk PdH_x. Source data are provided as a Source data file.

Preparation of supported NPs. We employed a common-used insert material, γ -Al₂O₃, as the support to anchor the Pd–FeO_x NPs (or Fe₃O₄ NPs, or Pd NPs). Typically, 200 mg of γ -Al₂O₃ was dispersed in a mixture of 15 mL of hexane and 20 mL of ethanol under sonication. A total of 20 mg of prepared NPs in 5 mL of hexane was added into the solution dropwise under sonication. The final mixture was further sonicated for 2 h and then magnetically stirred overnight. Subsequently, the NPs/Al₂O₃ was separated by centrifugation at 6082 × *g* for 10 min, and washed by 20 mL of ethanol and hexane for two times. The final sample was dried at 50 °C under vacuum overnight.

Preparation of Pd-Fe₃O₄-H and Pd-Fe₃O₄-A. The Pd-Fe₃O₄-H sample was prepared as follows: the Pd-FeO_x NPs/Al₂O₃ (ST2 NPs/Al₂O₃) was placed in a tube furnace and then heated to 300 °C at a ramping rate of 20 °C min⁻¹ and kept there for 1 h under the atmosphere of 4% H₂ in Ar atmosphere. The sample obtained was denoted as Pd-Fe₃O₄-H. The Pd amount was determined to be 0.171 wt.% by ICP. The Pd-Fe₃O₄-A sample was prepared by treating the Pd-FeO_x NPs/Al₂O₃ (ST2 NPs/Al₂O₃) in air under the same reaction condition.

Preparation of Pd-Fe₃O₄-Re. The Pd-Fe₃O₄-Re sample was prepared by treating Pd-Fe₃O₄-H in the air for another 1 h.

Preparation of Fe₃O₄-H. The Fe₃O₄-H sample was prepared by the same process of preparation of Pd–Fe₃O₄-H by using FeO_x NPs/Al₂O₃ instead of Pd–FeO_x NPs/Al₂O₃.

Preparation of control samples with different STs. Control samples with different ST were obtained by a similar synthesis process of Pd-FeO_x NPs using different amounts of Pd NPs seeds (37.5, 12.5, and 6.25 mg), the samples were respectively denoted as ST1 NPs, ST2 NPs, and ST3 NPs. The NPs were then deposited on the *y*-Al₂O₃ and further treated in the atmosphere of 4% H₂ in Ar for 1 h according to the same process of Pd-Fe₃O₄-H. (ST2 is the Pd-Fe₃O₄-H sample in this work).

Preparation of control samples with different structures. The control samples with different structures were prepared according to a similar process of Pd-Fe₃O₄-H at different annealing temperatures. The annealing temperature was 200 °C, 300 °C, and 400 °C, and the corresponding samples were denoted as T200, T300, and T400 (T300 is the Pd-Fe₃O₄-H sample in this work).

Characterization. The powder X-ray diffraction (XRD) patterns were collected on a PANalytical X'Pert Pro MPD diffractometer using an X'Celerator RTMS detector. HAADF-STEM and HR-STEM were performed on a Nion Ultra STEM 100 (operated at 100 kV). EELS spectra were collected on a high-resolution Gatan-Enfina ER with a probe size of 1.3 Å. TEM and high-angle annular bright-field scanning transmission electron microscopy (HAABF-STEM) were obtained on a Hitachi HD-200 with bright-field STEM detector operating at 200 kV.

The dispersion of the Pd was evaluated via pulse H₂-Chemisorption with an Altamira Instruments (AMI-300) system. Before the measurements, ~100 mg catalyst was pretreated at 550 °C for 3 h under 50 sccm of Ar, followed by cooling down to desired temperature (i.e., -130 and 35 °C) under the same flow. Then pulses of 4% H₂/Ar from a sample loop with a defined volume (~0.5 cc) were injected by switching a six-way valve until the eluted peak area of consecutive pulses was constant. The dispersion of Pd was calculated from the volume of H₂.

INS experiments were performed at the VISION beamline of the Spallation Neutron Source, Oak Ridge National Laboratory. The Pd- Fe_3O_4 -H sample was first treated under vacuum at 600 °C for 12 h. It was then loaded in an aluminum

sample holder in a helium glovebox. The sample holder was attached to a gasloading sample stick connected to a gas panel. The blank sample was first measured at -268 °C for 3 h to collect baseline spectrum. H₂ gas was then introduced in situ at -238 °C, followed by heating of the sample to -98 °C for reaction. The system was then cooled back to -268 °C to measure the reacted spectrum. The difference spectrum (reacted minus baseline) shows the signal associated with the hydride species formed during the reaction. The CO DRIFTS results were obtained on a Nicolet 670 Fourier Transform Infrared Spectrometer with an MCT detector by the following process: each sample (~15 mg) was loaded and then pretreated at 200 °C under Ar for 30 min. Afterward, the sample was cooled down to -120 °C to conduct CO adsorption. When the temperature reached -120 °C, the background was measured and then CO adsorption was conducted for 30 min as followed by desorption with Ar for 10 min (CO desorbed within 1 min after flow Ar). XPS characterization was performed on a PHI VersaProbe III scanning XPS microscope using a monochromatic Al K-alpha X-ray source (1486.6 eV). XPS spectra were acquired with 200 µm/50 W/15 kV X-ray settings and dual-beam charge neutralization. All binding energies were referenced to Al 2p peak at 74.8 eV.

Catalytic performance tests. The hydrogenation of C_2H_2 was carried out in a tubular quartz reactor with a 0.25-inch diameter. In a typical run, ~15 mg of catalyst was mixed with 150 mg of 60–80 mesh quartz sand and placed in the center of the reactor. The catalyst bed was held by quartz wool at both ends and the reactor was loaded in a vertical furnace (Carbolite Gero). The catalyst was purged with He for 30 min at a flow rate of 20 sccm prior to the reaction under room temperature. Then, the reactor was heated to the desired temperature (i.e., $30-80^{\circ}$ C), followed by feeding the gas mixture (i.e., $0.6 \text{ sccm } C_2H_2$, $3 \text{ sccm } H_2$ balanced with He) at a total flow rate of 50 sccm. The exit gas mixture was analyzed on-line by a ThermoStar Mass Spectrometry (Pfeiffer).

The conversion and selectivity were calculated by using Eqs. (1) and (2):

$$C_2H_2 \text{ Conversion}(\%) = \left(1 - \frac{X_{C_2H_2,out}}{X_{C_2H_2,in}}\right) \times 100\%$$
(1)

Selectivity(%) =
$$\frac{X_{C_2H_4,out}}{X_{C_2H_2,in} - X_{C_2H_2,out}} \times 100\%$$
 (2)

whereas in/out refers to the concentration measured in the inlet/outlet port.

Reaction orders with respect to H_2 and C_2H_2 were calculated by the differential method. The corresponding conversion is maintained below 20% to ensure a true kinetic regime. Apparent activation energy is calculated by the Arrhenius equation.

DFT calculation. The density functional theory calculations were performed with the Vienna Ab Initio Simulation Package (VASP)^{49,50}. The on-site Coulomb interaction was included with the DFT + U method by Dudarev et al.⁵¹ in VASP using a Hubbard parameter U = 3.8 eV for the Fe atom. The

Perdew-Burke-Ernzerhof⁵² functional form of generalized-gradient approximation was used for electron exchange and correlation energies. The projector augmented-wave method was used to describe the electron-core interaction^{49,53}. A kinetic energy cutoff of 450 eV was used for the plane waves. A $3 \times 2 \times 1$ sampling of Brillouin zone using a Monkhorst-Pack scheme was used⁵⁴. A vacuum layer of 15 Å was added for the surface slabs along the z-direction; the slab contains a total of four layers, with the bottom two layers fixed in their bulk positions.

XAFS data collection and processing. Approximately 20 mg of sample was enclosed in a nylon washer of 4.953 nm inner diameter and sealed on one side with transparent "Scotch" tape. The sample was pressed by hand to form a uniform pallet, then sealed on the open side with a tape. XAFS investigation were performed

at beamline 10ID-B of the Advanced Photon Source at Argonne National laboratory⁵⁵. Spectra were collected at the iron K-edge (7112 eV) and palladium Kedge (24,350 eV) in transmission mode, with an iron and palladium foil as a reference for energy calibration, respectively. All spectra were collected at room temperature and ten scans were collected for each sample. All data were processed and analyzed using the Athena and Artemis program of the IFFEFFIT package⁵ based on FEFF 6.0. Reference foil data were aligned to the first zero-crossing of the second derivative of the normalized $\mu(E)$ data, which was subsequently calibrated to the literature Eo for each Fe K-edge and Pd K-edge. The background was removed, and the data were assigned a Rbkg value of 1.0 prior to normalizing to obtain a unit edge step. All data were initially fit with k-weighting of 1, 2, and 3 then finalized with k³-weighting in R-space. A fit of the Pd foil and Fe foil was used to determine S₀² for each sample. Structure models used to fit the data sets were obtained from crystal structure of iron oxide and DFT calculation. Structure parameters that were determined by the fits include the degeneracy of the scattering path (N_{degen}), the change in Reff, the mean square relative displacement of the scattering element(σ_i^2), and the energy shift of the photoelectron(ΔE_0). k³weighting in R-space. Initial fitting was conducted using crystal structure from crystal database. The simulated models were obtained from DFT calculation and scattering paths of selected scattered atom (Fe, Pd) were generated through FEFF calculation. The WT method was adapted for a quantitative analysis of the backscattering atom in the higher coordination shells with EvAX code⁵⁷.

Data availability

The data that support the plots within this paper and other findings of this study are available from the corresponding author upon reasonable request. Source data are provided with this paper.

Received: 12 January 2020; Accepted: 13 May 2020; Published online: 16 June 2020

References

- Karim, W. et al. Catalyst support effects on hydrogen spillover. Nature 541, 68–71 (2017).
- Shan, J., Li, M., Allard, L. F., Lee, S. & Flytzani-Stephanopoulos, M. Mild oxidation of methane to methanol or acetic acid on supported isolated rhodium catalysts. *Nature* 551, 605–608 (2017).
- Dann, E. K. et al. Structural selectivity of supported Pd nanoparticles for catalytic NH3 oxidation resolved using combined operando spectroscopy. *Nat. Catal.* 2, 157–163 (2019).
- O'Connor, N. J., Jonayat, A. S. M., Janik, M. J. & Senftle, T. P. Interaction trends between single metal atoms and oxide supports identified with density functional theory and statistical learning. *Nat. Catal.* 1, 531–539 (2018).
- Zhao, M. et al. Metal-organic frameworks as selectivity regulators for hydrogenation reactions. *Nature* 539, 76–80 (2016).
- 6. Liu, L. et al. Generation of subnanometric platinum with high stability during transformation of a 2D zeolite into 3D. *Nat. Mater.* **16**, 132–138 (2017).
- Suchorski, Y. et al. The role of metal/oxide interfaces for long-range metal particle activation during CO oxidation. *Nat. Mater.* 17, 519–522 (2018).
- Huang, Y.-B., Liang, J., Wang, X.-S. & Cao, R. Multifunctional metal-organic framework catalysts: synergistic catalysis and tandem reactions. *Chem. Soc. Rev.* 46, 126–157 (2017).
- Zhang, J. & Zhao, C. Development of a bimetallic Pd-Ni/HZSM-5 catalyst for the tandem limonene dehydrogenation and fatty acid deoxygenation to alkanes and arenes for use as biojet fuel. ACS Catal. 6, 4512–4525 (2016).
- Li, S. et al. Tuning the selectivity of catalytic carbon dioxide hydrogenation over Iridium/Cerium oxide catalysts with a strong metal-support interaction. *Angew. Chem. Int. Ed.* 56, 10761–10765 (2017).
- Zhao, E. W. et al. Strong metal-support interactions enhance the pairwise selectivity of parahydrogen addition over Ir/TiO₂. ACS Catal. 6, 974–978 (2016).
- Tauster, S. J. & Fung, S. C. Strong metal-support interactions: occurrence among the binary oxides of groups IIA–VB. J. Catal. 55, 29–35 (1978).
- Tauster, S. J., Fung, S. C. & Garten, R. L. Strong metal-support interactions. Group 8 noble metals supported on titanium dioxide. J. Am. Chem. Soc. 100, 170–175 (1978).
- Tauster, S. J., Fung, S. C., Baker, R. T. K. & Horsley, J. A. Strong interactions in supported-metal catalysts. *Science* 211, 1121–1125 (1981).
- Zhang, J. et al. Wet-chemistry strong metal-support interactions in titaniasupported Au catalysts. J. Am. Chem. Soc. 141, 2975–2983 (2019).
- 16. Tang, H. et al. Classical strong metal-support interactions between gold nanoparticles and titanium dioxide. *Sci. Adv.* **3**, e1700231 (2017).
- Tang, H. et al. Strong metal-support interactions between gold nanoparticles and nonoxides. J. Am. Chem. Soc. 138, 56–59 (2016).

- Baker, L. R. et al. Furfuraldehyde hydrogenation on titanium oxide-supported platinum nanoparticles studied by sum frequency generation vibrational spectroscopy: acid-base catalysis explains the molecular origin of strong metal-support interactions. J. Am. Chem. Soc. 134, 14208–14216 (2012).
- Dong, J., Fu, Q., Jiang, Z., Mei, B. & Bao, X. Carbide-supported Au catalysts for water-gas shift reactions: a new territory for the strong metal-support interaction effect. J. Am. Chem. Soc. 140, 13808–13816 (2018).
- Lei, H. et al. Galvanic replacement-mediated synthesis of Ni-supported Pd nanoparticles with strong metal-support interaction for methanol electrooxidation. *Small* 15, 1804722 (2019).
- Kast, P. et al. Strong metal-support interaction and alloying in Pd/ZnO catalysts for CO oxidation. *Catal. Today* 260, 21–31 (2016).
- Tang, H. et al. Ultrastable hydroxyapatite/titanium-dioxide-supported gold nanocatalyst with strong metal-support interaction for carbon monoxide oxidation. *Angew. Chem. Int. Ed.* 55, 10606–10611 (2016).
- 23. Liu, S. et al. Ultrastable Au nanoparticles on titania through an encapsulation strategy under oxidative atmosphere. *Nat. Commun.* **10**, 5790 (2019).
- Matsubu, J. C. et al. Adsorbate-mediated strong metal-support interactions in oxide-supported Rh catalysts. *Nat. Chem.* 9, 120–127 (2017).
- Macino, M. et al. Tuning of catalytic sites in Pt/TiO₂ catalysts for the chemoselective hydrogenation of 3-nitrostyrene. *Nat. Catal.* 873–881 (2019).
- Liu, X. et al. Optimizing the structural configuration of FePt-FeO_x nanoparticles at the atomic scale by tuning the post-synthetic conditions. *Nano Energy* 55, 441–446 (2019).
- Liu, F. et al. Exchange-coupled fct-FePd/α-Fe nanocomposite magnets converted from Pd/Fe₃O₄ core/shell nanoparticles. *Chem. Eur. J.* 20, 15197–15202 (2014).
- Jang, J. W. et al. Enhancing charge carrier lifetime in metal oxide photoelectrodes through mild hydrogen treatment. *Adv. Energ. Mater.* 7, 1701536 (2017).
- Doudin, N. et al. Understanding heterolytic H₂ cleavage and water-assisted hydrogen spillover on Fe₃O₄(001)-supported single palladium atoms. ACS Catal. 9, 7876–7887 (2019).
- Hao, R., Fan, Y., Howard, M. D., Vaughan, J. C. & Zhang, B. Imaging nanobubble nucleation and hydrogen spillover during electrocatalytic water splitting. *Proc. Natl Acad. Sci. USA* 115, 5878–5883 (2018).
- Wu, C. H. et al. Bimetallic synergy in cobalt-palladium nanocatalysts for CO oxidation. *Nat. Catal.* 2, 78–85 (2018).
- Guo, Z., Kang, X., Zheng, X., Huang, J. & Chen, S. PdCu alloy nanoparticles supported on CeO₂ nanorods: Enhanced electrocatalytic activity by synergy of compressive strain, PdO and oxygen vacancy. *J. Catal.* 374, 101–109 (2019).
- Kast, P. et al. CO oxidation as a test reaction for strong metal-support interaction in nanostructured Pd/FeO powder catalysts. *Appl. Catal. A Gen.* 502, 8–17 (2015).
- 34. Wu, C.-T. et al. A non-syn-gas catalytic route to methanol production. *Nat. Commun.* **3**, 1050 (2012).
- Benziger, J. B. & Larson, L. R. An infrared spectroscopy study of the adsorption of CO on Fe/MgO. J. Catal. 77, 550–553 (1982).
- Felicissimo, M. P., Martyanov, O. N., Risse, T. & Freund, H.-J. Characterization of a Pd–Fe bimetallic model catalyst. *Surf. Sci.* 601, 2105–2116 (2007).
- Wei, X., Ma, Z., Lu, J., Mu, X. & Hu, B. Strong metal-support interactions between palladium nanoclusters and hematite toward enhanced acetylene dicarbonylation at low temperature. *N. J. Chem.* 44, 1221–1227 (2020).
- Teschner, D. et al. The roles of subsurface carbon and hydrogen in palladiumcatalyzed alkyne hydrogenation. *Science* **320**, 86–89 (2008).
- 39. Teschner, D. et al. Understanding Palladium hydrogenation catalysts: When the nature of the reactive molecule controls the nature of the catalyst active phase. *Angew. Chem. Int. Ed.* **47**, 9274–9278 (2008).
- Schneemann, A. et al. Nanostructured metal hydrides for hydrogen storage. Chem. Rev. 118, 10775–10839 (2018).
- Zhang, Y., Diao, W., Williams, C. T. & Monnier, J. R. Selective hydrogenation of acetylene in excess ethylene using Ag- and Au–Pd/SiO₂ bimetallic catalysts prepared by electroless deposition. *Appl. Catal. A Gen.* 469, 419–426 (2014).
- Takht Ravanchi, M., Sahebdelfar, S. & Rahimi Fard, M. Influence of support structural characteristics on long-term performance of Pd-Ag/α-Al₂O₃ catalyst for tail-end acetylene selective hydrogenation. *Int. J. Chem. React. Eng.* 14, 1035–1046 (2016).
- Vincent, M. J. & Gonzalez, R. D. A Langmuir–Hinshelwood model for a hydrogen transfer mechanism in the selective hydrogenation of acetylene over a Pd/γ-Al₂O₃ catalyst prepared by the sol–gel method. *Appl. Catal. A Gen.* 217, 143–156 (2001).
- Molero, H., Bartlett, B. F. & Tysoe, W. T. The hydrogenation of acetylene catalyzed by palladium: hydrogen pressure dependence. *J. Catal.* 181, 49–56 (1999).
- 45. Pei, G. X. et al. Ag alloyed Pd single-atom catalysts for efficient selective hydrogenation of acetylene to ethylene in excess ethylene. *ACS Catal.* **5**, 3717–3725 (2015).

ARTICLE

- Adúriz, H. R., Bodnariuk, P., Dennehy, M. & Gigola, C. E. Activity and selectivity of Pd/α-Al₂O₃ for ethyne hydrogenation in a large excess of ethene and hydrogen. *Appl. Catal.* 58, 227–239 (1990).
- Tan, S., Cheng, Y. Q., Daemen, L. L. & Lutterman, D. A. Design of a facility for the in situ measurement of catalytic reaction by neutron scattering spectroscopy. *Rev. Sci. Instrum.* 89, 014101 (2018).
- Polo-Garzon, F. et al. Neutron scattering investigations of hydride species in heterogeneous catalysis. *Chemsuschem* 12, 93–103 (2019).
- Kresse, G. & Furthmuller, J. Efficiency of ab-initio total energy calculations for metals and semiconductors using a plane-wave basis set. *Comput. Mater. Sci.* 6, 15–50 (1996).
- Kresse, G. & Furthmuller, J. Efficient iterative schemes for ab initio total-energy calculations using a plane-wave basis set. *Phys. Rev. B* 54, 11169–11186 (1996).
- Dudarev, S., Botton, G., Savrasov, S., Humphreys, C. & Sutton, A. electronenergy-loss spectra and the structural stability of nickel oxide: an LSDA+ U study. *Phys. Rev. B* 57, 1505–1509 (1998).
- Perdew, J. P., Burke, K. & Ernzerhof, M. Generalized gradient approximation made simple. *Phys. Rev. Lett.* 77, 3865–3868 (1996).
- 53. Blöchl, P. E. Projector augmented-wave method. *Phys. Rev. B* **50**, 17953–17979 (1994).
- Monkhorst, H. J. & Pack, J. D. Special points for Brillouin-zone integrations. *Phys. Rev. B* 13, 5188–5192 (1976).
- 55. The MRCAT Insertion Device Beamline at the Advanced Photon Source", C.U. Segre, N.E. Leyarovska, L.D. Chapman, W.M. Lavender, P.W. Plag, A.S. King, A.J. Kropf, B.A. Bunker, K.M. Kemner, P. Dutta, R.S. Duran and J. Kaduk, CP521, Synchrotron Radiation Instrumentation: Eleventh U.S. National Conference, (ed. P. Pianetta, et al.) p419–422, (American Insitute of Physics, New York, 2000).
- Ravel, B. & Newville, M. ATHENA, ARTEMIS, HEPHAESTUS: data analysis for X-ray absorption spectroscopy using IFEFFIT. J. Synchrotron Radiat. 12, 537–541 (2005).
- Timoshenko, J., Kuzmin, A. & Purans, J. EXAFS study of hydrogen intercalation into ReO₃ using the evolutionary algorithm. *J. Phy. Condens. Mat.* 26, 055401 (2014).

Acknowledgements

This research is sponsored by the U.S. Department of Energy (DOE), Office of Science, Office of Basic Energy Sciences, Chemical Sciences, Geosciences, and Biosciences Division, Catalysis Science Program. The computational calculations used resources of the National Energy Research Scientific Computing Center, a DOE Office of Science User Facility. XAFS data were collected at the Advanced Photon Source at Argonne National Laboratory on Beamline 10ID-B, supported by the Materials Research Collaborative Access Team (MRCAT). MRCAT operations are supported by the DOE and the MRCAT member institutions. This research used resources of the Advanced Photon Source, a U.S. DOE Office of Science User Facility operated for the DOE Office of Science by Argonne National Laboratory under contract no. DE-AC02-06CH11357. The neutron studies used resources at the Spallation Neutron Source, a DOE Office of Science User Facility operated by Oak Ridge National Laboratory. Part of the work including the chemisorption was conducted at the Center for Nanophase Materials Sciences, which is a DOE Office of Science User Facility. The Spallation Neutron Source at Oak Ridge National Laboratory is supported by the Scientific User Facilities Division, Office of Basic Energy Sciences, U.S. DOE, under contract no. DE-AC0500OR22725 with UT Battelle, LLC. Part of the TEM work was performed at the Center for Functional Nanomaterials, Brookhaven National Laboratory, which is supported by the U.S. DOE, Office of Basic Energy

Science, under contract no. DE-SC0012704. P.W.W., W.S.Z., and H.M.L. were financially supported by the National Natural Science Foundation of China (21722604), Natural Science Foundation of Jiangsu Province (BK20190852). P.W.W. is thankful to the scholarship from China Scholarship Council (CSC).

Author contributions

H.Y.Z., P.W.W., S.T., and S.D. conceived the idea of the work. P.W.W. synthesized the samples and carried out the XRD analysis. S.T. performed the catalytic experiments. J.M. and C.W.A. performed the XAFS. J.M., V.F., D.E.J., P.W.W., H.Y.Z., and C.W.A. analyzed the XAFS result, and carried out the DFT simulation. J.M. performed the CO DRIFTS. P.W.W. and H.Y.Z. analyzed the CO DRIFTS results. N.L., D.S., and S.Z.Y. performed the part of the TEM, HAADF-STEM, STEM, HR-STEM, and EELS mapping. P.W.W. and H.Y.Z. performed some of the TEM characterizations. N.L., P.W.W., W.S.Z., Z.H.Y., and H.Y.Z. analyzed the microscopic results. Y.Q.C. and Z.L.W. carried out the INS characterization, and analyzed the results. S.T. performed H₂-chemisorption characterization. P.W.W., S.T., A.S., A.M.M., H.M.L., Z.H.Y., W.S.Z., S.D., and H.Y.Z. discussed the results. Z.H.Y., P.W.W., and H.Y.Z. analyzed the manuscript. All authors modified the manuscript. P.W.W., S.T., and H.Y.Z. finalized the manuscript.

Competing interests

The authors declare no competing interests.

Additional information

Supplementary information is available for this paper at https://doi.org/10.1038/s41467-020-16674-y.

Correspondence and requests for materials should be addressed to W.Z., S.D. or H.Z.

Peer review information *Nature Communications* thanks Meenakshisundaram Sankar and the other, anonymous, reviewer(s) for their contribution to the peer review of this work. Peer reviewer reports are available.

Reprints and permission information is available at http://www.nature.com/reprints

Publisher's note Springer Nature remains neutral with regard to jurisdictional claims in published maps and institutional affiliations.

Open Access This article is licensed under a Creative Commons Attribution 4.0 International License, which permits use, sharing, adaptation, distribution and reproduction in any medium or format, as long as you give appropriate credit to the original author(s) and the source, provide a link to the Creative Commons license, and indicate if changes were made. The images or other third party material in this article are included in the article's Creative Commons license, unless indicated otherwise in a credit line to the material. If material is not included in the article's Creative Commons license and your intended use is not permitted by statutory regulation or exceeds the permitted use, you will need to obtain permission directly from the copyright holder. To view a copy of this license, visit http://creativecommons.org/ licenses/by/4.0/.

© The Author(s) 2020